

CO₂ Removal using a Synthetic Analogue of Carbonic Anhydrase

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Program Team



- Hamilton Sundstrand
 Review of CO₂ separations system testing
- Columbia University
 Modification of Synthetic Analogue
 (Prof. Gerard Parkin's group)
- WorleyParsons, LLC
 Review of power plant -coupled system performance and cost models
- CM-Tec, Inc.

 Custom Chemical Synthesis
- GL Chemtec Int'l, Ltd.

 Custom Chemical Synthesis
- · Consultants:



Prof. Benny Freeman University of Texas



Prof. William Koros Georgia Tech













Prof. Don Paul University of Texas



Prof. E. Bryan Coughlin UMass (Amherst)



CO₂ Capture for Space Applications



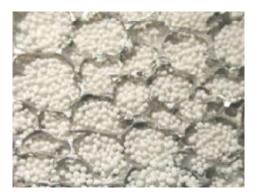
Hamilton-Sundstrand is NASA's prime contractor for CO₂ capture in space

- CAMRAS: CO₂ And Moisture Removal Amine Swing bed
- Prototype delivered to NASA JSC (currently TRL6)
- Baselined for Orion; Lunar Lander; and new space suit
- Regeneration by space vacuum (heat for Mars environment)
- Heat exchange between adsorption/desorption maintains system isothermal





Volunteers and NASA JSC scientists testing the CAMRAS system



HS solid amine sorbent in metal foam



Prototype CAMRAS system



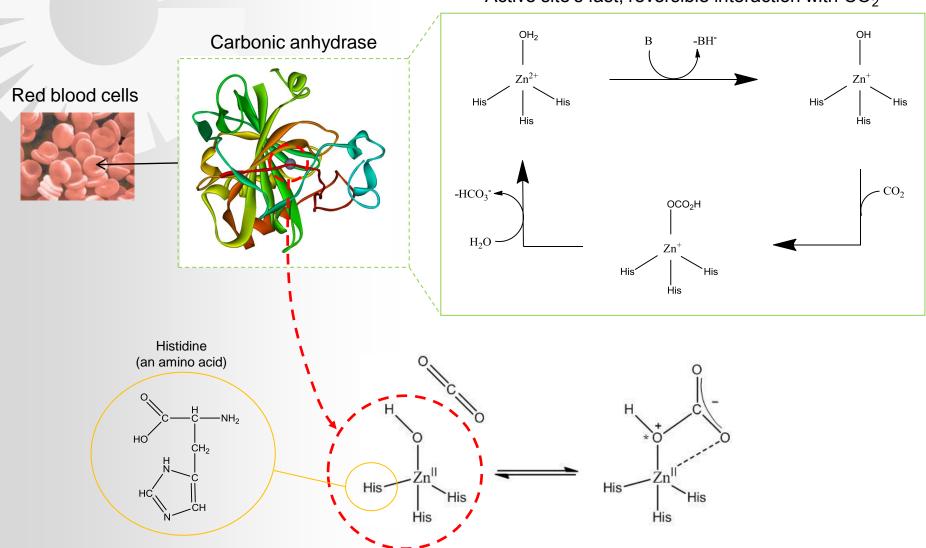


Carbonic Anhydrase: Nature's Solution



What we can learn from the enzyme: reactive, coordinated ZnOH site

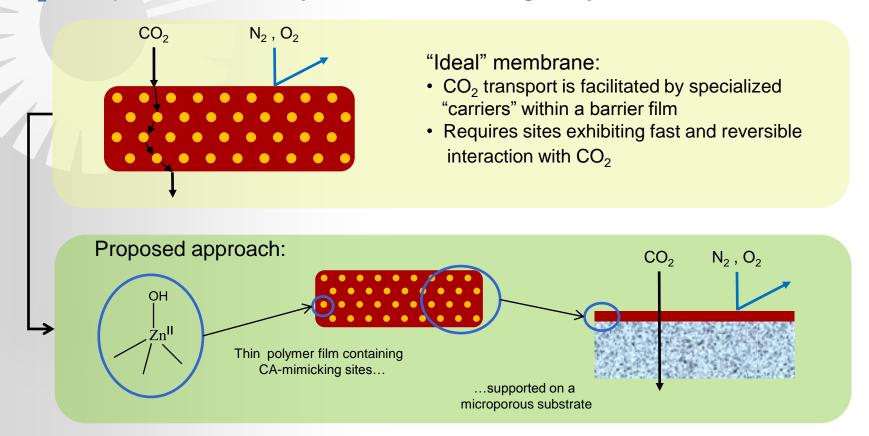
Active site's fast, reversible interaction with CO₂



Proposed Approach: Membrane-based Separation



CO₂ transport facilitated by carriers mimicking enzyme active site



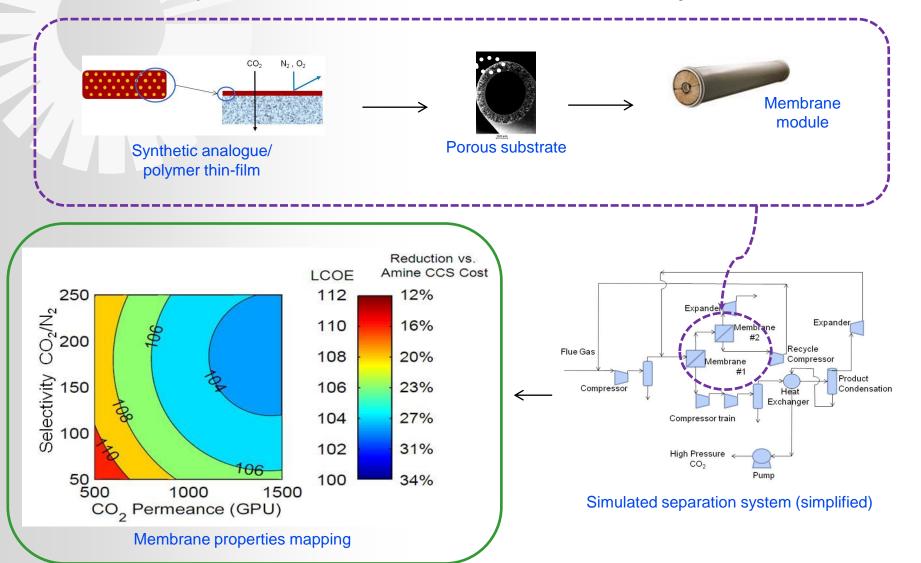
- ~30% lower CO₂ capture cost compared to liquid amines
- ~2 billion tons/yr CO₂ from existing coal-fired power plants
- Modular, skid-mounted configurations; no moving parts
- Flexibility to start with smaller system, gradually increase to 90% CO₂ capture



Separation System Feasibility Study



Simulation compares membrane vs. benchmark amine system





Resistance to Flue Gas Contaminants: Experiments



Analogue (powder) exposed in liquid and gas phase at max. expected levels

Coal Type	SO ₂	NO ₂	NO	HCI
Sub-bituminous	27.7	4.0	76.0	0.28
Bituminous "A"	78.5	4.3	81.7	3.44
Bituminous "B"	55.5	4.5	85.7	4.15
Bituminous "C"	38.2	3.3	61.8	9.9
Lignite "A"	68.2	3.5	67.3	0.34
Lignite "B"	123.8	4.5	84.6	0.03

(Highest concentration at each coal type noted in red)

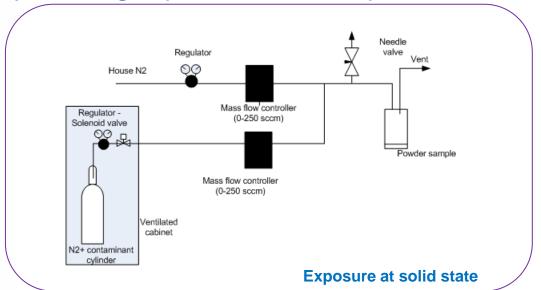


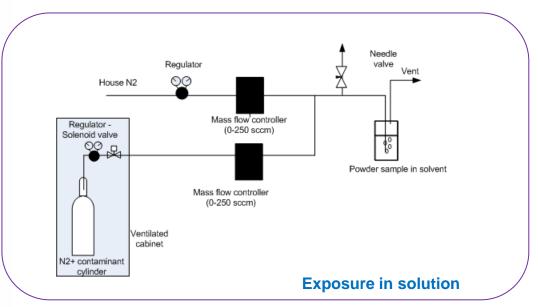
SO₂: 125ppm & 12ppm

NO₂: 35ppm (~10X)

NO: 85ppm

HCI: 10ppm, ~50% RH







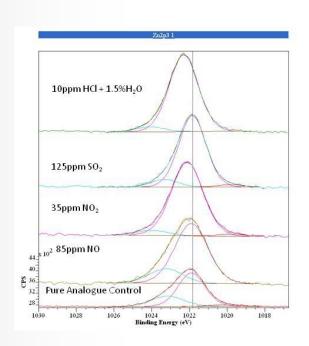
Exposure to Flue Gas Contaminants: Results

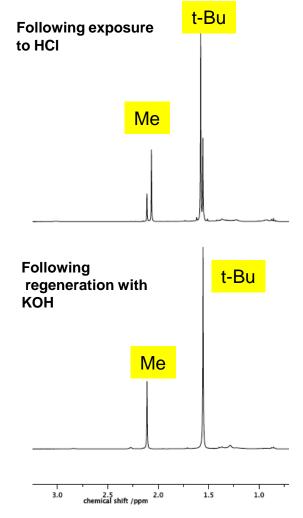


Interactions with NO2, SO2 & HCI possible but reversible

- No evidence of structural or active site degradation
- Shifts in NMR & XPS (Zn) peaks observed with SO₂, NO₂ & HCl but not with NO.
- Original NMR peaks restored following treatment in liquid phase (KOH) and gas phase.

Zinc binding energy shifts (indicating active site stability)





¹H NMR spectra of [Tp^{But,Me}]ZnOH following exposure to HCl



Key Findings to Date:



A separation system based on a membrane having both high selectivity and permeance can compare favorably to current benchmark (liquid amines)

Three of the four main flue gas contaminants could form a reaction product with the synthetic analogue but the membrane can be regenerated

Incorporation of the ZnOH active site in the grafted synthetic analogue has proved more difficult than anticipated and and has delayed progress.



Synthetic Analogue Modification Examples



Incorporate functional units for grafting or (co)polymerization COOR COOR COOR COOR Path 1: Replace –H with -COOH Path 2: Replace Me with double bond







CO₂ Capture with Enzyme Synthetic Analogue



